

UNIVERSITI SAINS MALAYSIA

Peperiksaan Semester Pertama
Sidang Akademik 1997/98

September 1997

EMK 101 - Termodinamik

Masa : [3 jam]

ARAHAN KEPADA CALON:

Sila pastikan bahawa kertas peperiksaan ini mengandungi **ENAM** muka surat, **TIGA BELAS** lampiran dan **ENAM** soalan yang bercetak sebelum anda memulakan peperiksaan ini.

Jawab **LIMA** soalan sahaja.

Semua jawapan **MESTILAH** dijawab di dalam Bahasa Malaysia.

Jawapan untuk setiap soalan **MESTI** dimulakan pada muka surat yang berasingan.

Termasuk Lampiran:

1. Jadual Stim

...2/-

S1. [a] Berikan takrifan-takrifan berikut:

- [i] Proses boleh balik
- [ii] Kitar termodinamik
- [iii] Haba
- [iv] Kerja berlaku
- [v] Hukum pertama termodinamik

(15 markah)

[b] Bendalir pada suhu 150°C dan tekanan 1 bar dimampatkan secara isoterma ke isipadu tentu $0.28 \text{ m}^3/\text{kg}$. Tentukan per kg bendalir.

- [i] perubahan tenaga dalam
- [ii] perubahan entropi
- [iii] pemindahan haba
- [iv] kerja berlaku

bagi:

- [i] stim
- [ii] udara

Lukiskan proses tersebut ke atas gambarajah P-v.

Data bagi udara:

$$\begin{aligned} C_p &= 1.005 \text{ kJ/kgK} \\ C_v &= 0.718 \text{ kJ/kgK} \end{aligned}$$

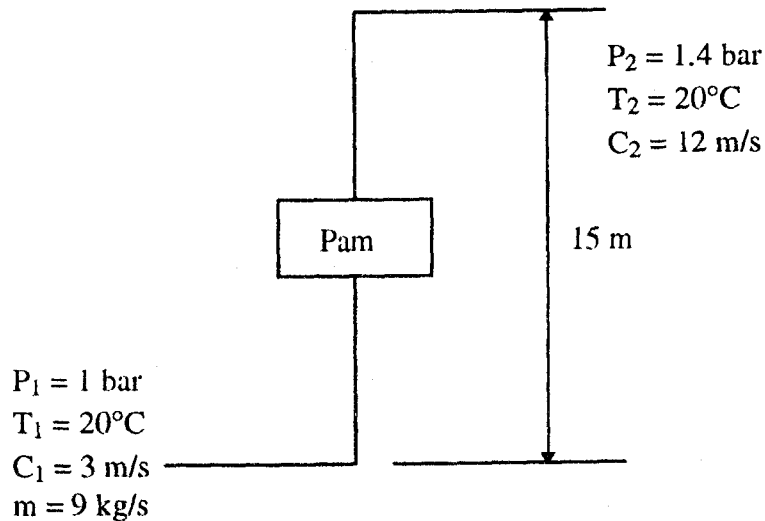
(85 markah)

S2. [a] Stim memasuki sebuah turbin dengan kadar alir jisim 4600 kg/jam . Turbin tersebut menjana 1000 kW . Di alur masuk tekanannya 60 bar, suhu 400°C dan halaju 10 m/s . Di alur keluar tekanannya 0.1 bar, kualiti wap 90% dan halaju 50 m/s . Tentukan pemindahan haba di antara turbin dan keliling. Lukiskan proses tersebut ke atas gambarajah T-v.

(50 markah)

...3/-

[b] Timbangkan Rajah S2[b] di bawah.



Rajah S2[b]

Tentukan kuasa yang diperlukan oleh pam untuk mengepam air ke tahap 15 m. Andaikan pecutan graviti 10 m/s^2 dan pemindahan haba bolehabai.

(50 markah)

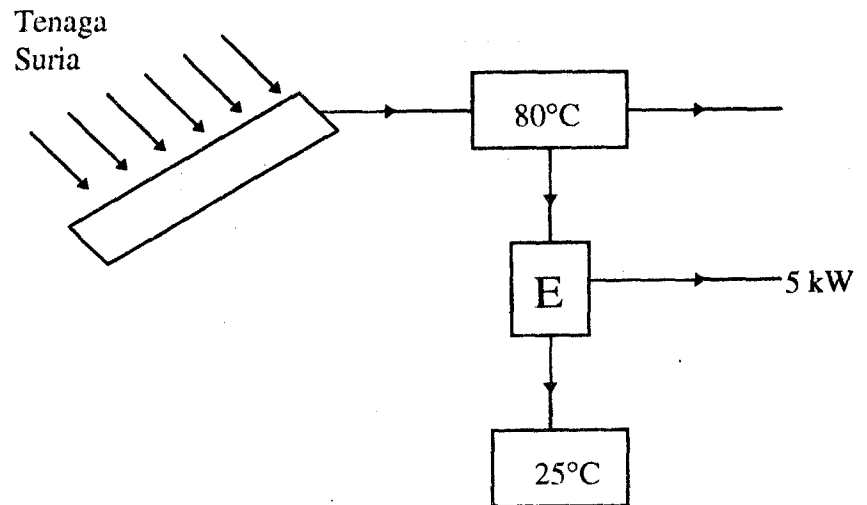
S3. [a] Nyatakan kenyataan Clausius yang merupakan salah satu siratan hukum II dan buktikan bahawa semua enjin haba yang dikendali di antara 2 takungan yang sama mempunyai kecekapan yang sama.

(20 markah)

[b] Sebuah enjin haba boleh balik menerima tenaga daripada sebuah pengumpul suria pada suhu 80°C dan membuang haba ke keliling pada suhu 25°C . Lihat Rajah S3[b]. Pengumpul suria menukar 50 peratus tenaga suria tertuju kepada tenaga yang berguna. Jika 1 kW tenaga suria menyinari 1 m^2 luas pengumpul, apakah luas pengumpul yang diperlukan untuk membekal 5 kW kuasa keluaran daripada enjin haba.

(80 markah)

...4/-

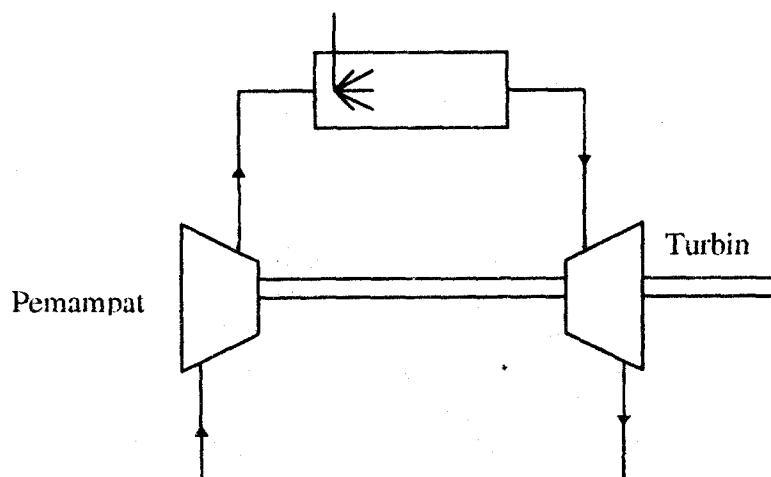


Rajah S3[b]

- S4. [a] Apakah yang dimaksudkan dengan tekanan berkesan min dan tunjukkan contoh berdasarkan kitar Diesel.

(15 markah)

- [b] Sebuah loji gas turbin digunakan untuk menjana kuasa. Rajah S4[b] menunjukkan kitar terbuka Brayton.



Rajah S4[b]

...5/-

Suhu maksimum kitar adalah 1000 K dan suhu minimum 288 K. Nisbah tekanan adalah 6. Kecekapan isentropi bagi pemampat adalah 85 % dan kecekapan isentropi turbin adalah 90 %.

- [i] Lukiskan gambarajah T-s dan p-v bagi kitar tersebut
- [ii] Tentukan kecekapan loji tersebut
- [iii] Tentukan nisbah kerja

Data bagi udara $C_p = 1.005 \text{ kJ/kg K}$
 $C_v = 0.718 \text{ kJ/kg K}$

(85 markah)

- S5. [a] Berikan tiga sebab kenapa kitar Carnot tidak sesuai digunakan bagi loji stim

(15 markah)

- [b] Stim digunakan sebagai bendalir di dalam kitar Rankine yang mempunyai pemanas semula dan pemanas lampau. Kitar ini dikendalikan di antara tekanan 30 bar dan 0.04 bar. Darjah panas lampau stim yang memasuki turbin pertama ialah 216.1°C . Di dalam turbin pertama stim berkembang hingga menjadi wap tepu. Kemudian stim dipanas semula ke suhu 450°C sebelum memasuki turbin kedua. Andaikan kerja pam suap bolehabai, tentukan:

- [i] kecekapan kitar Rankine
- [ii] penggunaan stim tentu

Lukiskan gambarajah T-s bagi kitar tersebut.

(85 markah)

...6/-

- S6. [a] Kitar mampatan wap berdasarkan kitar terbalik Carnot. Terangkan kenapa turbin yang digunakan bagi kitar terbalik Carnot ditukarkan kepada pendikit. Kenapa proses penyejukan di dalam kitar mampatan wap diteruskan hingga ke wap tepu sebelum proses mampatan.

(15 markah)

- [b] Bahan pendingin R12 digunakan di dalam kitar penyejukan mampatan wap. Wap tepu memasuki pemampat pada 12°C . Cecair tepu meninggalkan pemeluwap pada tekanan 1.4 MPa. Pemampat mempunyai kecekapan 80%. Kadar alir jisim bahan pendingin ialah 0.008 kg/s. Tentukan:

- [i] Kuasa mampatan di dalam kW
- [ii] Muatan penyejukan
- [iii] Pekali prestasi

Lukiskan gambarajah T-s.

Terangkan secara ringkas bagaimana muatan penyejukan boleh dipertingkatkan.

(85 markah)

Saturated Water and Steam

t [°C]	p_s [bar]	v_g [m³/kg]	h_f	h_{fg} [kJ/kg]	h_g	s_f	s_{fg} [kJ/kg K]	s_g
0.01	0.006112	206.1	0*	2500.8	2500.8	0†	9.155	9.155
1	0.006566	192.6	4.2	2498.3	2502.5	0.015	9.113	9.128
2	0.007054	179.9	8.4	2495.9	2504.3	0.031	9.071	9.102
3	0.007575	168.2	12.6	2493.6	2506.2	0.046	9.030	9.076
4	0.008129	157.3	16.8	2491.3	2508.1	0.061	8.989	9.050
5	0.008719	147.1	21.0	2488.9	2509.9	0.076	8.948	9.024
6	0.009346	137.8	25.2	2486.6	2511.8	0.091	8.908	8.999
7	0.01001	129.1	29.4	2484.3	2513.7	0.106	8.868	8.974
8	0.01072	121.0	33.6	2481.9	2515.5	0.121	8.828	8.949
9	0.01147	113.4	37.8	2479.6	2517.4	0.136	8.788	8.924
10	0.01227	106.4	42.0	2477.2	2519.2	0.151	8.749	8.900
11	0.01312	99.90	46.2	2474.9	2521.1	0.166	8.710	8.876
12	0.01401	93.83	50.4	2472.5	2522.9	0.180	8.671	8.851
13	0.01497	88.17	54.6	2470.2	2524.8	0.195	8.633	8.828
14	0.01597	82.89	58.8	2467.8	2526.6	0.210	8.594	8.804
15	0.01704	77.97	62.9	2465.5	2528.4	0.224	8.556	8.780
16	0.01817	73.38	67.1	2463.1	2530.2	0.239	8.518	8.757
17	0.01936	69.09	71.3	2460.8	2532.1	0.253	8.481	8.734
18	0.02063	65.08	75.5	2458.4	2533.9	0.268	8.444	8.712
19	0.02196	61.34	79.7	2456.0	2535.7	0.282	8.407	8.689
20	0.02337	57.84	83.9	2453.7	2537.6	0.296	8.370	8.666
21	0.02486	54.56	88.0	2451.4	2539.4	0.310	8.334	8.644
22	0.02642	51.49	92.2	2449.0	2541.2	0.325	8.297	8.622
23	0.02808	48.62	96.4	2446.6	2543.0	0.339	8.261	8.600
24	0.02982	45.92	100.6	2444.2	2544.8	0.353	8.226	8.579
25	0.03166	43.40	104.8	2441.8	2546.6	0.367	8.190	8.557
26	0.03360	41.03	108.9	2439.5	2548.4	0.381	8.155	8.536
27	0.03564	38.81	113.1	2437.2	2550.3	0.395	8.120	8.515
28	0.03778	36.73	117.3	2434.8	2552.1	0.409	8.085	8.494
29	0.04004	34.77	121.5	2432.4	2553.9	0.423	8.050	8.473
30	0.04242	32.93	125.7	2430.0	2555.7	0.436	8.016	8.452
32	0.04754	29.57	134.0	2425.3	2559.3	0.464	7.948	8.412
34	0.05318	26.60	142.4	2420.5	2562.9	0.491	7.881	8.372
36	0.05940	23.97	150.7	2415.8	2566.5	0.518	7.814	8.332
38	0.06624	21.63	159.1	2411.0	2570.1	0.545	7.749	8.294
40	0.07375	19.55	167.5	2406.2	2573.7	0.572	7.684	8.256
42	0.08198	17.69	175.8	2401.4	2577.2	0.599	7.620	8.219
44	0.09100	16.03	184.2	2396.6	2580.8	0.625	7.557	8.182
46	0.1009	14.56	192.5	2391.8	2584.3	0.651	7.494	8.145
48	0.1116	13.23	200.9	2387.0	2587.9	0.678	7.433	8.111
50	0.1233	12.04	209.3	2382.1	2591.4	0.704	7.371	8.075
55	0.1574	9.578	230.2	2370.1	2600.3	0.768	7.223	7.991
60	0.1992	7.678	251.1	2357.9	2609.0	0.831	7.078	7.909
65	0.2501	6.201	272.0	2345.7	2617.7	0.893	6.937	7.830
70	0.3116	5.045	293.0	2333.3	2626.3	0.955	6.800	7.755
75	0.3855	4.133	313.9	2320.8	2634.7	1.015	6.666	7.681
80	0.4736	3.408	334.9	2308.3	2643.2	1.075	6.536	7.611
85	0.5780	2.828	355.9	2295.6	2651.5	1.134	6.410	7.544
90	0.7011	2.361	376.9	2282.8	2659.7	1.192	6.286	7.478
95	0.8453	1.982	398.0	2269.8	2667.8	1.250	6.166	7.416
100	1.01325	1.673	419.1	2256.7	2675.8	1.307	6.048	7.355

† u and s are chosen to be zero for saturated liquid at the triple point.Note: values of v_f can be found on p. 10.

Saturated Water and Steam

p [bar]	t_s [°C]	v_g [m³/kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
0.006112	0.01	206.1	0†	2375	0*	2501	2501	0†	9.155	9.155
0.010	7.0	129.2	29	2385	29	2485	2514	0.106	8.868	8.974
0.015	13.0	87.98	55	2393	55	2470	2525	0.196	8.631	8.827
0.020	17.5	67.01	73	2399	73	2460	2533	0.261	8.462	8.723
0.025	21.1	54.26	88	2403	88	2451	2539	0.312	8.330	8.642
0.030	24.1	45.67	101	2408	101	2444	2545	0.354	8.222	8.576
0.035	26.7	39.48	112	2412	112	2438	2550	0.391	8.130	8.521
0.040	29.0	34.80	121	2415	121	2433	2554	0.422	8.051	8.473
0.045	31.0	31.14	130	2418	130	2428	2558	0.451	7.980	8.431
0.050	32.9	28.20	138	2420	138	2423	2561	0.476	7.918	8.394
0.055	34.6	25.77	145	2422	145	2419	2564	0.500	7.860	8.360
0.060	36.2	23.74	152	2425	152	2415	2567	0.521	7.808	8.329
0.065	37.7	22.02	158	2427	158	2412	2570	0.541	7.760	8.301
0.070	39.0	20.53	163	2428	163	2409	2572	0.559	7.715	8.274
0.075	40.3	19.24	169	2430	169	2405	2574	0.576	7.674	8.250
0.080	41.5	18.10	174	2432	174	2402	2576	0.593	7.634	8.227
0.085	42.7	17.10	179	2434	179	2400	2579	0.608	7.598	8.206
0.090	43.8	16.20	183	2435	183	2397	2580	0.622	7.564	8.186
0.095	44.8	15.40	188	2436	188	2394	2582	0.636	7.531	8.167
0.100	45.8	14.67	192	2437	192	2392	2584	0.649	7.500	8.149
0.12	49.4	12.36	207	2442	207	2383	2590	0.696	7.389	8.085
0.14	52.6	10.69	220	2446	220	2376	2596	0.737	7.294	8.031
0.16	55.3	9.432	232	2450	232	2369	2601	0.772	7.213	7.985
0.18	57.8	8.444	242	2453	242	2363	2605	0.804	7.140	7.944
0.20	60.1	7.648	251	2456	251	2358	2609	0.832	7.075	7.907
0.22	62.2	6.994	260	2459	260	2353	2613	0.858	7.016	7.874
0.24	64.1	6.445	268	2461	268	2348	2616	0.882	6.962	7.844
0.26	65.9	5.979	276	2464	276	2343	2619	0.904	6.913	7.817
0.28	67.5	5.578	283	2466	283	2339	2622	0.925	6.866	7.791
0.30	69.1	5.228	289	2468	289	2336	2625	0.944	6.823	7.767
0.32	70.6	4.921	295	2470	295	2332	2627	0.962	6.783	7.745
0.34	72.0	4.649	302	2472	302	2328	2630	0.980	6.745	7.725
0.36	73.4	4.407	307	2473	307	2325	2632	0.996	6.709	7.705
0.38	74.7	4.189	312	2475	312	2322	2634	1.011	6.675	7.686
0.40	75.9	3.992	318	2476	318	2318	2636	1.026	6.643	7.669
0.42	77.1	3.814	323	2478	323	2315	2638	1.040	6.612	7.652
0.44	78.2	3.651	327	2479	327	2313	2640	1.054	6.582	7.636
0.46	79.3	3.502	332	2481	332	2310	2642	1.067	6.554	7.621
0.48	80.3	3.366	336	2482	336	2308	2644	1.079	6.528	7.607
0.50	81.3	3.239	340	2483	340	2305	2645	1.091	6.502	7.593
0.55	83.7	2.964	351	2486	351	2298	2649	1.119	6.442	7.561
0.60	86.0	2.731	360	2489	360	2293	2653	1.145	6.386	7.531
0.65	88.0	2.535	369	2492	369	2288	2657	1.169	6.335	7.504
0.70	90.0	2.364	377	2494	377	2283	2660	1.192	6.286	7.478
0.75	91.8	2.217	384	2496	384	2278	2662	1.213	6.243	7.456
0.80	93.5	2.087	392	2498	392	2273	2665	1.233	6.201	7.434
0.85	95.2	1.972	399	2500	399	2269	2668	1.252	6.162	7.414
0.90	96.7	1.869	405	2502	405	2266	2671	1.270	6.124	7.394
0.95	98.2	1.777	411	2504	411	2262	2673	1.287	6.089	7.376
1.00	99.6	1.694	417	2506	417	2258	2675	1.303	6.056	7.359

$$\frac{h_f}{\text{kJ/kg}} = \frac{p v_f}{\text{kJ/kg}} = \frac{p}{\text{bar}} \times \frac{10^5 \text{ N}}{\text{m}^2} \times \frac{v_f}{\text{m}^3/\text{kg}} \times \left[\frac{\text{m}^3}{\text{kg}} \right] \times \frac{[\text{kJ}]}{10^3 \text{ N m}} \times \frac{1}{[\text{kJ/kg}]}$$

$$= \frac{p}{\text{bar}} \times \frac{v_f}{\text{m}^3/\text{kg}} \times 10^2 = 0.006112 \times 0 \times 10002 \times 10^2 = 0.0006112$$

Saturated Water and Steam

p [bar]	t_s [°C]	v_g [m³/kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
1.0	99.6	1.694	417	2506	417	2253	2675	1.303	6.056	7.359
1.1	102.3	1.549	429	2510	429	2251	2680	1.333	5.994	7.327
1.2	104.8	1.428	439	2512	439	2244	2683	1.361	5.937	7.298
1.3	107.1	1.325	449	2515	449	2233	2687	1.387	5.884	7.271
1.4	109.3	1.236	458	2517	458	2232	2690	1.411	5.835	7.246
1.5	111.4	1.159	467	2519	467	2225	2693	1.434	5.789	7.223
1.6	113.3	1.091	475	2521	475	2221	2696	1.455	5.747	7.202
1.7	115.2	1.031	483	2524	483	2215	2699	1.475	5.707	7.182
1.8	116.9	0.9774	491	2526	491	2211	2702	1.494	5.669	7.163
1.9	118.6	0.9292	498	2528	498	2205	2704	1.513	5.632	7.145
2.0	120.2	0.8856	505	2530	505	2202	2707	1.530	5.597	7.127
2.1	121.8	0.8461	511	2531	511	2198	2709	1.547	5.564	7.111
2.2	123.3	0.8100	518	2533	518	2193	2711	1.563	5.533	7.096
2.3	124.7	0.7770	524	2534	524	2189	2713	1.578	5.503	7.081
2.4	126.1	0.7466	530	2536	530	2185	2715	1.593	5.474	7.067
2.5	127.4	0.7186	535	2537	535	2182	2717	1.607	5.446	7.053
2.6	128.7	0.6927	541	2539	541	2178	2719	1.621	5.419	7.040
2.7	130.0	0.6686	546	2540	546	2174	2720	1.634	5.393	7.027
2.8	131.2	0.6462	551	2541	551	2171	2722	1.647	5.368	7.015
2.9	132.4	0.6253	556	2543	556	2168	2724	1.660	5.344	7.004
3.0	133.5	0.6057	561	2544	561	2164	2725	1.672	5.321	6.993
3.5	138.9	0.5241	584	2549	584	2148	2732	1.727	5.214	6.941
4.0	143.6	0.4623	605	2554	605	2134	2739	1.776	5.121	6.897
4.5	147.9	0.4139	623	2558	623	2121	2744	1.820	5.037	6.857
5.0	151.8	0.3748	639	2562	640	2109	2749	1.860	4.962	6.827
5.5	155.3	0.3427	655	2565	656	2097	2753	1.897	4.893	6.790
6	158.8	0.3156	669	2568	670	2087	2757	1.931	4.830	6.761
7	165.0	0.2728	696	2573	697	2067	2764	1.992	4.717	6.709
8	170.4	0.2403	720	2577	721	2048	2769	2.046	4.617	6.663
9	175.4	0.2149	742	2581	743	2031	2774	2.094	4.529	6.623
10	179.9	0.1944	762	2584	763	2015	2778	2.138	4.448	6.586
11	184.1	0.1774	780	2586	781	2000	2781	2.179	4.375	6.554
12	188.0	0.1632	797	2588	798	1986	2784	2.216	4.307	6.523
13	191.6	0.1512	813	2590	815	1972	2787	2.251	4.244	6.495
14	195.0	0.1408	828	2593	830	1960	2790	2.284	4.185	6.469
15	198.3	0.1317	843	2595	845	1947	2792	2.315	4.130	6.445
16	201.4	0.1237	857	2596	859	1935	2794	2.344	4.078	6.422
17	204.3	0.1167	870	2597	872	1923	2795	2.372	4.028	6.400
18	207.1	0.1104	883	2598	885	1912	2797	2.398	3.981	6.379
19	209.8	0.1047	895	2599	897	1901	2798	2.423	3.936	6.359
20	212.4	0.09957	907	2600	909	1890	2799	2.447	3.895	6.340
22	217.2	0.09069	928	2601	931	1870	2801	2.492	3.815	6.305
24	221.8	0.08323	949	2602	952	1850	2802	2.534	3.738	6.272
26	226.0	0.07689	969	2603	972	1831	2803	2.574	3.668	6.242
28	230.0	0.07142	988	2603	991	1812	2803	2.611	3.602	6.213
30	233.8	0.06665	1004	2603	1008	1795	2803	2.645	3.541	6.186
32	237.4	0.06246	1021	2603	1025	1778	2803	2.679	3.482	6.161
34	240.9	0.05875	1038	2603	1042	1761	2803	2.710	3.426	6.136
36	244.2	0.05544	1054	2602	1058	1744	2802	2.740	3.373	6.113
38	247.3	0.05246	1068	2602	1073	1729	2802	2.769	3.322	6.091
40	250.3	0.04977	1082	2602	1087	1714	2801	2.797	3.273	6.070

Saturated Water and Steam

p [bar]	t_s [°C]	v_g [m³/kg]	u_f [kJ/kg]	u_g [kJ/kg]	h_f [kJ/kg]	h_{fg} [kJ/kg]	h_g [kJ/kg]	s_f [kJ/kg K]	s_{fg} [kJ/kg K]	s_g [kJ/kg K]
40	250.3	0.04977	1082	2602	1087	1714	2801	2.797	3.273	6.070
42	253.2	0.04732	1097	2601	1102	1698	2800	2.823	3.226	6.049
44	256.0	0.04509	1109	2600	1115	1683	2798	2.849	3.180	6.029
46	258.8	0.04305	1123	2599	1129	1668	2797	2.874	3.136	6.010
48	261.4	0.04117	1136	2598	1142	1654	2796	2.897	3.094	5.991
50	263.9	0.03944	1149	2597	1155	1639	2794	2.921	3.052	5.973
55	269.9	0.03563	1178	2594	1185	1605	2790	2.976	2.955	5.931
60	275.6	0.03244	1206	2590	1214	1570	2784	3.027	2.863	5.890
65	280.8	0.02972	1232	2586	1241	1538	2779	3.076	2.775	5.851
70	285.8	0.02737	1258	2581	1267	1505	2772	3.122	2.692	5.814
75	290.5	0.02532	1283	2576	1293	1473	2766	3.166	2.613	5.779
80	295.0	0.02352	1306	2570	1317	1441	2758	3.207	2.537	5.744
85	299.2	0.02192	1329	2565	1341	1410	2751	3.248	2.463	5.711
90	303.3	0.02048	1351	2559	1364	1379	2743	3.286	2.393	5.679
95	307.2	0.01919	1372	2552	1386	1348	2734	3.324	2.323	5.647
100	311.0	0.01802	1393	2545	1408	1317	2725	3.360	2.255	5.615
105	314.6	0.01696	1414	2537	1429	1286	2715	3.395	2.189	5.584
110	318.0	0.01598	1434	2529	1450	1255	2705	3.430	2.123	5.553
115	321.4	0.01508	1454	2522	1471	1224	2695	3.463	2.060	5.523
120	324.6	0.01426	1473	2514	1491	1194	2685	3.496	1.997	5.493
125	327.8	0.01349	1492	2505	1511	1163	2674	3.529	1.934	5.463
130	330.8	0.01278	1511	2496	1531	1131	2662	3.561	1.872	5.433
135	333.8	0.01211	1530	2487	1551	1099	2650	3.592	1.811	5.403
140	336.6	0.01149	1548	2477	1571	1067	2638	3.623	1.750	5.373
145	339.4	0.01090	1567	2467	1591	1034	2625	3.654	1.689	5.343
150	342.1	0.01035	1585	2456	1610	1001	2611	3.685	1.627	5.312
155	344.8	0.00982	1604	2445	1630	967	2597	3.715	1.565	5.280
160	347.3	0.00932	1623	2433	1650	932	2582	3.746	1.502	5.248
165	349.8	0.00884	1641	2420	1670	895	2565	3.777	1.437	5.214
170	352.3	0.00838	1660	2406	1690	858	2548	3.808	1.373	5.181
175	354.6	0.00794	1679	2391	1711	819	2530	3.839	1.305	5.144
180	357.0	0.00751	1699	2375	1732	778	2510	3.872	1.236	5.108
185	359.2	0.00709	1719	2358	1754	735	2489	3.905	1.163	5.068
190	361.4	0.00668	1740	2339	1777	689	2466	3.941	1.086	5.027
195	363.6	0.00627	1762	2318	1801	639	2440	3.977	1.004	4.981
200	365.7	0.00585	1786	2294	1827	584	2411	4.014	0.914	4.928
202	366.5	0.00569	1796	2283	1838	560	2398	4.031	0.875	4.906
204	367.4	0.00552	1806	2271	1849	535	2384	4.049	0.835	4.884
206	368.2	0.00534	1817	2259	1861	508	2369	4.067	0.792	4.859
208	369.0	0.00517	1829	2245	1874	479	2353	4.087	0.745	4.832
210	369.8	0.00498	1842	2231	1889	447	2336	4.108	0.695	4.803
212	370.6	0.00479	1856	2214	1904	412	2316	4.131	0.640	4.771
214	371.4	0.00458	1871	2196	1921	373	2294	4.157	0.579	4.736
216	372.1	0.00436	1888	2174	1940	328	2268	4.186	0.508	4.694
218	372.9	0.00409	1911	2146	1965	270	2235	4.224	0.417	4.641
220	373.7	0.00368	1949	2097	2008	170	2178	4.289	0.263	4.552
221.2	374.15	0.00317	2014	2014	2084	0	2084	4.406	0.000	4.406

Superheated Steam

$p/[\text{bar}]$ ($t_s/^\circ\text{C}$)		t [$^\circ\text{C}$]	50	100	150	200	250	300	400	500
0	$u = h - RT$	v								
		u	2446	2517	2589	2662	2737	2812	2969	3132
		h	2595	2689	2784	2880	2978	3077	3280	3489
		s								
0.006112 (0.01)	v_g 206.1 u_g 2375 h_g 2501 s_g 9.155	v 243.9 u 2446 h 2595 s 9.468	281.7 2517 2689 9.739	319.5 2589 2784 9.978	357.3 2662 2880 10.193	395.0 2737 2978 10.390	432.8 2812 3077 10.571	508.3 2969 3280 10.897	583.8 3132 3489 11.187	
0.01 (7.0)	v_g 129.2 u_g 2385 h_g 2514 s_g 8.974	v 149.1 u 2446 h 2595 s 9.241	172.2 2517 2689 9.512	195.3 2589 2784 9.751	218.4 2662 2880 9.966	241.4 2737 2978 10.163	264.5 2812 3077 10.344	310.7 2969 3280 10.670	356.8 3132 3489 10.960	
0.05 (32.9)	v_g 28.20 u_g 2420 h_g 2561 s_g 8.394	v 29.78 u 2445 h 2594 s 8.496	34.42 2516 2688 8.768	39.04 2589 2784 9.008	43.66 2662 2880 9.223	48.28 2737 2978 9.420	52.90 2812 3077 9.601	62.13 2969 3280 9.927	71.36 3132 3489 10.217	
0.1 (45.8)	v_g 14.67 u_g 2437 h_g 2584 s_g 8.149	v 14.87 u 2443 h 2592 s 8.173	17.20 2516 2688 8.447	19.51 2588 2783 8.688	21.83 2662 2880 8.903	24.14 2736 2977 9.100	26.45 2812 3077 9.281	31.06 2969 3280 9.607	35.68 3132 3489 9.897	
0.5 (81.3)	v_g 3.239 u_g 2483 h_g 2645 s_g 7.593	v 3.420 u 2512 h 2683 s 7.694	3.890 2585 2780 7.940	4.356 2660 2878 8.158	4.821 2735 2976 8.355	5.284 2812 3076 8.537	6.209 2969 3279 8.864	7.134 3132 3489 9.154		
0.75 (91.8)	v_g 2.217 u_g 2496 h_g 2662 s_g 7.456	v 2.271 u 2510 h 2680 s 7.500	2.588 2585 2779 7.750	2.901 2659 2877 7.969	3.211 2734 2975 8.167	3.521 2811 3075 8.349	4.138 2968 3279 8.676	4.755 3132 3489 8.967		
1 (99.6)	v_g 1.694 u_g 2506 h_g 2675 s_g 7.359	v 1.696 u 2506 h 2676 s 7.360	1.937 2583 2777 7.614	2.173 2659 2876 7.834	2.406 2734 2975 8.033	2.639 2811 3075 8.215	2.969 2968 3278 8.543	3.565 3131 3488 8.834		
1.01325 (100.0)	v_g 1.673 u_g 2506 h_g 2676 s_g 7.355	v 1.912 u 2583 h 2777 s 7.608	2.145 2659 2876 7.828	2.375 2734 2975 8.027	2.604 2811 3075 8.209	2.837 2968 3277 8.537	3.519 3131 3488 8.828			
1.5 (111.4)	v_g 1.159 u_g 2519 h_g 2693 s_g 7.223	v 1.286 u 2580 h 2773 s 7.420	1.445 2656 2873 7.643	1.601 2733 2973 7.843	1.757 2809 3073 8.027	1.907 2967 3277 8.355	2.376 3131 3488 8.646			
2 (120.2)	v_g 0.8856 u_g 2530 h_g 2707 s_g 7.127	v 0.9602 u 2578 h 2770 s 7.280	1.081 2655 2871 7.507	1.199 2731 2971 7.708	1.316 2809 3072 7.892	1.549 2967 3277 8.221	1.781 3131 3487 8.513			
3 (133.5)	v_g 0.6057 u_g 2544 h_g 2725 s_g 6.993	v 0.6342 u 2572 h 2762 s 7.078	0.7166 2651 2866 7.312	0.7965 2729 2968 7.517	0.8754 2807 3070 7.702	1.021 2966 3275 8.032	1.187 3130 3486 8.324			
4 (143.6)	v_g 0.4623 u_g 2554 h_g 2739 s_g 6.897	v 0.4710 u 2565 h 2753 s 6.929	0.5345 2648 2862 7.172	0.5953 2727 2965 7.379	0.6549 2805 3067 7.566	0.7725 2965 3274 7.898	0.8893 3129 3485 8.191			

Superheated Steam

p/[bar] (t _s /[°C])		t [°C]		200	250	300	350	400	450	500	600
5 (151.8)	v _g	0.3748	v	0.4252	0.4745	0.5226	0.5701	0.6172	0.6641	0.7108	0.8040
	u _g	2562	u	2644	2725	2804	2883	2963	3045	3129	3300
	h _g	2749	h	2857	2962	3065	3168	3272	3377	3484	3702
	s _g	6.822	s	7.060	7.271	7.460	7.633	7.793	7.944	8.087	8.351
6 (158.8)	v _g	0.3156	v	0.3522	0.3940	0.4344	0.4743	0.5136	0.5528	0.5919	0.6697
	u _g	2568	u	2640	2722	2801	2881	2962	3044	3128	3299
	h _g	2757	h	2851	2958	3062	3166	3270	3376	3483	3701
	s _g	6.761	s	6.968	7.182	7.373	7.546	7.707	7.858	8.001	8.267
7 (165.0)	v _g	0.2728	v	0.3001	0.3364	0.3714	0.4058	0.4397	0.4734	0.5069	0.5737
	u _g	2573	u	2636	2720	2800	2880	2961	3043	3127	3298
	h _g	2764	h	2846	2955	3060	3164	3269	3374	3482	3700
	s _g	6.709	s	6.888	7.06	7.298	7.473	7.634	7.786	7.929	8.195
8 (170.4)	v _g	0.2403	v	0.2610	0.2933	0.3242	0.3544	0.3842	0.4138	0.4432	0.5018
	u _g	2577	u	2631	2716	2798	2878	2960	3042	3126	3298
	h _g	2769	h	2840	2951	3057	3162	3267	3373	3481	3699
	s _g	6.653	s	6.817	7.040	7.233	7.409	7.571	7.723	7.866	8.132
9 (175.4)	v _g	0.2149	v	0.2305	0.2597	0.2874	0.3144	0.3410	0.3674	0.3937	0.4458
	u _g	2581	u	2628	2714	2796	2877	2959	3041	3126	3298
	h _g	2774	h	2835	2948	3055	3160	3266	3372	3480	3699
	s _g	6.623	s	6.753	6.980	7.176	7.352	7.515	7.667	7.811	8.077
10 (179.9)	v _g	0.1944	v	0.2061	0.228	0.2580	0.2825	0.3065	0.3303	0.3540	0.4010
	u _g	2584	u	2623	2711	2794	2875	2957	3040	3124	3297
	h _g	2778	h	2828	2944	3052	3158	3264	3370	3478	3698
	s _g	6.586	s	6.695	6.926	7.124	7.301	7.464	7.617	7.761	8.028
15 (198.3)	v _g	0.1317	v	0.1324	0.1520	0.1697	0.1865	0.2029	0.2191	0.2351	0.2667
	u _g	2595	u	2597	2677	2784	2868	2952	3035	3120	3294
	h _g	2792	h	2796	2925	3039	3148	3256	3364	3473	3694
	s _g	6.445	s	6.452	6.711	6.919	7.102	7.268	7.423	7.569	7.838
20 (212.4)	v _g	0.0996	v		0.1115	0.1255	0.1386	0.1511	0.1634	0.1756	0.1995
	u _g	2600	u		2631	2774	2861	2946	3030	3116	3291
	h _g	2799	h		2944	3025	3138	3248	3357	3467	3690
	s _g	6.340	s		6.547	6.768	6.957	7.126	7.283	7.431	7.701
30 (233.8)	v _g	0.0666	v		0.0706	0.0812	0.0905	0.0993	0.1078	0.1161	0.1324
	u _g	2603	u		2616	2751	2845	2933	3020	3108	3285
	h _g	2803	h		2878	2995	3117	3231	3343	3456	3682
	s _g	6.186	s		6.289	6.541	6.744	6.921	7.082	7.233	7.507
40 (250.3)	v _g	0.0498	v			0.0588	0.0664	0.0733	0.0800	0.0864	0.0988
	u _g	2602	u			2728	2828	2921	3010	3099	3279
	h _g	2801	h			2963	3094	3214	3330	3445	3674
	s _g	6.070	s			6.364	6.584	6.769	6.935	7.089	7.368
50 (263.9)	v _g	0.0394	v			0.0453	0.0519	0.0578	0.0632	0.0685	0.0786
	u _g	2597	u			2700	2810	2907	3000	3090	3273
	h _g	2794	h			2927	3070	3196	3316	3433	3666
	s _g	5.973	s			6.212	6.451	6.646	6.818	6.975	7.258
60 (275.6)	v _g	0.0324	v			0.0362	0.0422	0.0473	0.0521	0.0566	0.0652
	u _g	2590	u			2670	2792	2893	2988	3081	3266
	h _g	2784	h			2887	3045	3177	3301	3421	3657
	s _g	5.890	s			6.071	6.336	6.541	6.719	6.879	7.166
70 (285.8)	v _g	0.0274	v			0.0295	0.0352	0.0399	0.0441	0.0481	0.0556
	u _g	2581	u			2634	2772	2879	2978	3073	3260
	h _g	2772	h			2841	3018	3158	3287	3410	3649
	s _g	5.814	s			5.934	6.231	6.448	6.622	6.796	7.088

Superheated Steam

p [bar] (t_s [°C])		t [°C]	350	375	400	425	450	500	600	700
80 (295.0)	v_g 0.02352 h_g 2758 s_g 5.744	$v \times 10^3$ h s	2.994 2990 6.133	3.220 3067 6.255	3.428 3139 6.364	3.625 3207 6.463	3.812 3272 6.555	4.170 3398 6.723	4.839 3641 7.019	5.476 3881 7.279
90 (303.3)	v_g 0.02048 h_g 2743 s_g 5.679	$v \times 10^3$ h s	2.578 2959 6.039	2.794 3042 6.171	2.991 3118 6.286	3.173 3189 6.390	3.346 3256 6.484	3.673 3385 6.657	4.279 3633 6.958	4.852 3874 7.220
100 (311.0)	v_g 0.01802 h_g 2725 s_g 5.615	$v \times 10^3$ h s	2.241 2926 5.947	2.453 3017 6.091	2.639 3097 6.213	2.812 3172 6.321	2.972 3241 6.419	3.275 3373 6.596	3.831 3624 6.902	4.353 3868 7.166
110 (318.0)	v_g 0.01598 h_g 2705 s_g 5.553	$v \times 10^3$ h s	1.960 2889 5.856	2.169 2989 6.014	2.350 3075 6.143	2.514 3153 6.257	2.666 3225 6.358	2.949 3360 6.539	3.465 3616 6.850	3.945 3862 7.117
120 (324.6)	v_g 0.01426 h_g 2685 s_g 5.493	$v \times 10^3$ h s	1.719 2849 5.762	1.931 2960 5.937	2.107 3052 6.076	2.265 3134 6.195	2.410 3209 6.301	2.677 3348 6.487	3.159 3607 6.802	3.605 3856 7.072
130 (330.8)	v_g 0.01278 h_g 2662 s_g 5.433	$v \times 10^3$ h s	1.509 2804 5.664	1.726 2929 5.862	1.901 3028 6.011	2.053 3114 6.136	2.193 3192 6.246	2.447 3335 6.437	2.901 3599 6.758	3.318 3850 7.030
140 (336.6)	v_g 0.01149 h_g 2638 s_g 5.373	$v \times 10^3$ h s	1.321 2753 5.559	1.548 2896 5.784	1.722 3003 5.946	1.872 3093 6.079	2.006 3175 6.193	2.250 3322 6.390	2.679 3590 6.716	3.071 3843 6.991
150 (342.1)	v_g 0.01035 h_g 2611 s_g 5.312	$v \times 10^3$ h s	1.146 2693 5.443	1.391 2861 5.707	1.566 2977 5.883	1.714 3073 6.023	1.844 3157 6.142	2.078 3309 6.345	2.487 3581 6.677	2.857 3837 6.954
160 (347.3)	v_g 0.00932 h_g 2582 s_g 5.248	$v \times 10^3$ h s	0.976 2617 5.304	1.248 2821 5.626	1.427 2949 5.820	1.573 3051 5.968	1.702 3139 6.093	1.928 3295 6.301	2.319 3573 6.639	2.670 3831 6.919
170 (352.3)	v_g 0.00838 h_g 2548 s_g 5.181	$v \times 10^3$ h s		1.117 2778 5.541	1.303 2920 5.756	1.449 3028 5.914	1.576 3121 6.044	1.796 3281 6.260	2.171 3564 6.603	2.506 3825 6.886
180 (357.0)	v_g 0.00751 h_g 2510 s_g 5.108	$v \times 10^3$ h s		0.997 2729 5.449	1.191 2888 5.691	1.338 3004 5.861	1.463 3102 5.997	1.678 3268 6.219	2.039 3555 6.569	2.359 3818 6.855
190 (361.4)	v_g 0.00668 h_g 2466 s_g 5.027	$v \times 10^3$ h s		0.882 2674 5.348	1.089 2855 5.625	1.238 2980 5.807	1.362 3082 5.950	1.572 3254 6.180	1.921 3546 6.536	2.228 3812 6.825
200 (365.7)	v_g 0.00585 h_g 2411 s_g 4.928	$v \times 10^3$ h s		0.768 2605 5.228	1.095 2819 5.556	1.270 2955 5.753	1.477 3062 5.904	1.719 3239 6.142	2.110 3537 6.505	2.403 3806 6.796
210 (369.8)	v_g 0.00498 h_g 2336 s_g 4.803	$v \times 10^3$ h s		0.650 2500 5.050	1.064 2781 5.484	1.270 2928 5.699	1.477 3041 5.859	1.719 3225 6.105	2.110 3528 6.474	2.403 3799 6.768
220 (373.7)	v_g 0.00368 h_g 2178 s_g 4.552	$v \times 10^3$ h s		0.450 2300 4.725	1.064 2738 5.409	1.270 2900 5.645	1.477 3020 5.813	1.719 3210 6.068	2.110 3519 6.444	2.403 3793 6.742
221.2 (374.15)	v_g 0.00317 h_g 2084 s_g 4.406	$v \times 10^3$ h s		0.163 1637 3.708	0.351 2139 4.490	0.816 2723 5.398	0.978 2896 5.638	1.103 3017 5.807	1.303 3208 6.064	1.622 3518 6.441

Linear interpolation is not accurate near the critical point.

$$E_{572} = 3564 - \left(\frac{3564 - 3281}{3564 - 3281} \right) (3564 - 3281)$$

Supercritical Steam

$\frac{p}{\text{[bar]}}$	$\frac{t}{\text{[}^\circ\text{C]}}$	350	375	400	425	450	500	600	700	800
225	$v \times 10^3$	0.163	0.249	0.786	0.951	1.076	1.275	1.591	1.861	2.109
	h	1635	1980	2716	2885	3009	3203	3514	3790	4055
	s	3.704	4.470	5.369	5.616	5.790	6.050	6.430	6.729	6.988
250	$v \times 10^3$	0.160	0.198	0.601	0.789	0.917	1.113	1.412	1.662	1.890
	h	1625	1850	2580	2807	2951	3165	3491	3774	4043
	s	3.682	4.026	5.142	5.474	5.677	5.962	6.361	6.667	6.931
275	$v \times 10^3$	0.158	0.187	0.419	0.650	0.786	0.980	1.265	1.500	1.710
	h	1617	1811	2382	2718	2890	3125	3468	3758	4032
	s	3.662	3.985	4.828	5.320	5.562	5.878	6.296	6.610	6.878
300	$v \times 10^3$	0.155	0.180	0.282	0.530	0.674	0.868	1.143	1.364	1.561
	h	1610	1791	2157	2614	2823	3084	3445	3742	4020
	s	3.645	3.923	4.482	5.157	5.444	5.795	6.234	6.557	6.829
350	$v \times 10^3$	0.152	0.171	0.211	0.343	0.496	0.693	0.952	1.152	1.327
	h	1599	1762	1992	2375	2673	2998	3397	3709	3997
	s	3.614	3.875	4.219	4.776	5.197	5.633	6.120	6.459	6.741
400	$v \times 10^3$	0.149	0.164	0.191	0.255	0.369	0.562	0.809	0.993	1.152
	h	1590	1743	1935	2203	2514	2906	3348	3677	3974
	s	3.588	3.832	4.119	4.510	4.947	5.474	6.014	6.371	6.662
450	$v \times 10^3$	0.146	0.160	0.181	0.219	0.291	0.463	0.698	0.870	1.016
	h	1583	1729	1901	2115	2380	2813	3299	3644	3951
	s	3.565	3.777	4.056	4.368	4.740	5.320	5.914	6.290	6.590
500	$v \times 10^3$	0.144	0.156	0.173	0.201	0.249	0.388	0.611	0.772	0.908
	h	1577	1717	1879	2064	2288	2722	3249	3612	3928
	s	3.544	3.758	4.009	4.279	4.594	5.176	5.821	6.214	6.524
550	$v \times 10^3$	0.143	0.153	0.168	0.190	0.224	0.334	0.540	0.693	0.820
	h	1572	1709	1862	2030	2227	2641	3200	3579	3905
	s	3.525	3.742	3.971	4.218	4.494	5.047	5.731	6.144	6.462
600	$v \times 10^3$	0.141	0.151	0.164	0.182	0.209	0.295	0.483	0.627	0.747
	h	1568	1702	1848	2005	2184	2571	3152	3548	3883
	s	3.506	3.718	3.939	4.168	4.419	4.937	5.648	6.077	6.405
650	$v \times 10^3$	0.139	0.148	0.160	0.176	0.198	0.267	0.436	0.572	0.685
	h	1565	1676	1837	1986	2151	2514	3106	3517	3860
	s	3.489	3.697	3.910	4.128	4.360	4.845	5.568	6.014	6.352
700	$v \times 10^3$	0.138	0.146	0.157	0.171	0.189	0.247	0.397	0.526	0.633
	h	1561	1671	1829	1971	2127	2468	3062	3486	3839
	s	3.473	3.678	3.886	4.093	4.312	4.769	5.494	5.955	6.300
750	$v \times 10^3$	0.137	0.145	0.154	0.167	0.183	0.231	0.365	0.486	0.587
	h	1559	1667	1821	1958	2107	2431	3021	3456	3817
	s	3.459	3.659	3.863	4.064	4.272	4.705	5.425	5.899	6.252
800	$v \times 10^3$	0.136	0.143	0.152	0.163	0.178	0.219	0.338	0.452	0.548
	h	1557	1664	1815	1948	2091	2400	2983	3428	3797
	s	3.444	3.642	3.842	4.037	4.237	4.651	5.361	5.845	6.206
900	$v \times 10^3$	0.133	0.140	0.148	0.158	0.169	0.202	0.296	0.396	0.484
	h	1554	1658	1805	1932	2066	2353	2916	3373	3756
	s	3.418	3.612	3.805	3.991	4.179	4.563	5.248	5.746	6.120
1000	$v \times 10^3$	0.131	0.138	0.145	0.153	0.163	0.189	0.267	0.354	0.434
	h	1552	1654	1798	1920	2048	2319	2860	3324	3718
	s	3.394	3.584	3.773	3.951	4.131	4.493	5.153	5.656	6.042

Saturated Water and Steam

t [°C]	p_s [bar]	v_f $10^{-2}[\text{m}^3/\text{kg}]$	c_{pf} [kJ/kg K]	c_{ps} [kJ/kg K]	μ_f $10^{-6}[\text{kg}/\text{m s}]$	μ_g $10^{-6}[\text{kg}/\text{m s}]$	k_f $10^{-8}[\text{kW}/\text{m K}]$	k_g $10^{-8}[\text{kW}/\text{m K}]$	$(Pr)_f$	$(Pr)_g$
0.01	0.006112	0.10002	4.210	1.86	1752	8.49	569	16.3	12.96	0.97
5	0.008719	0.10001	4.204	1.86	1501	8.66	578	16.7	10.92	0.96
10	0.01227	0.10003	4.193	1.86	1300	8.83	587	17.1	9.29	0.96
15	0.01704	0.10010	4.186	1.87	1136	9.00	595	17.5	7.99	0.96
20	0.02337	0.10018	4.183	1.87	1002	9.18	603	17.9	6.95	0.96
25	0.03166	0.10030	4.181	1.88	890	9.35	611	18.3	6.09	0.96
30	0.04242	0.10044	4.179	1.88	797	9.52	618	18.7	5.39	0.96
35	0.05622	0.10060	4.178	1.88	718	9.70	625	19.1	4.80	0.96
40	0.07375	0.10079	4.179	1.89	651	9.87	632	19.5	4.30	0.96
45	0.09582	0.10099	4.181	1.89	594	10.0	638	19.9	3.89	0.95
50	0.1233	0.1012	4.182	1.90	544	10.2	643	20.4	3.54	0.95
55	0.1574	0.1015	4.183	1.90	501	10.4	648	20.8	3.23	0.95
60	0.1992	0.1017	4.185	1.91	463	10.6	653	21.2	2.97	0.95
65	0.2501	0.1020	4.188	1.92	430	10.7	658	21.6	2.74	0.95
70	0.3116	0.1023	4.191	1.93	400	10.9	662	22.0	2.53	0.96
75	0.3855	0.1026	4.194	1.94	374	11.1	666	22.5	2.36	0.96
80	0.4736	0.1029	4.198	1.95	351	11.3	670	22.9	2.20	0.96
85	0.5780	0.1032	4.203	1.96	330	11.4	673	23.3	2.06	0.96
90	0.7011	0.1036	4.208	1.97	311	11.6	676	23.8	1.94	0.96
95	0.8453	0.1040	4.213	1.99	294	11.8	678	24.3	1.83	0.97
100	1.01325	0.1044	4.219	2.01	279	12.0	681	24.8	1.73	0.97
105	1.208	0.1048	4.226	2.03	265	12.2	683	25.3	1.64	0.98
110	1.433	0.1052	4.233	2.05	252	12.4	684	25.8	1.56	0.99
115	1.691	0.1056	4.240	2.07	241	12.6	686	26.3	1.49	0.99
120	1.985	0.1060	4.248	2.09	230	12.8	687	26.8	1.42	1.00
125	2.321	0.1065	4.26	2.12	220	13.0	687	27.3	1.36	1.01
130	2.701	0.1070	4.27	2.15	211	13.2	688	27.8	1.31	1.02
135	3.131	0.1075	4.28	2.18	203	13.4	688	28.3	1.26	1.03
140	3.614	0.1080	4.29	2.21	195	13.5	688	28.8	1.22	1.04
145	4.155	0.1085	4.30	2.25	188	13.7	687	29.4	1.18	1.05
150	4.760	0.1091	4.32	2.29	181	13.9	687	30.0	1.14	1.07
160	6.181	0.1102	4.35	2.38	169	14.2	684	31.3	1.07	1.09
170	7.920	0.1114	4.38	2.49	159	14.6	681	32.6	1.02	1.12
180	10.03	0.1128	4.42	2.62	149	15.0	676	34.1	0.97	1.15
190	12.55	0.1142	4.46	2.76	141	15.3	671	35.7	0.94	1.18
200	15.55	0.1157	4.51	2.91	134	15.7	665	37.5	0.91	1.22
210	19.08	0.1173	4.56	3.07	127	16.0	657	39.4	0.88	1.25
220	23.20	0.1190	4.63	3.25	121	16.3	648	41.5	0.86	1.28
230	27.98	0.1209	4.70	3.45	116	16.7	639	43.9	0.85	1.31
240	33.48	0.1229	4.78	3.68	111	17.1	628	46.5	0.84	1.35
250	39.78	0.1251	4.87	3.94	107	17.5	616	49.5	0.85	1.39
260	46.94	0.1276	4.98	4.22	103	17.9	603	52.8	0.85	1.43
270	55.05	0.1302	5.10	4.55	99	18.3	589	56.6	0.86	1.47
280	64.19	0.1332	5.24	4.98	96	18.8	574	61.0	0.88	1.53
290	74.45	0.1366	5.42	5.46	93	19.3	558	66.0	0.90	1.60
300	85.92	0.1404	5.65	6.18	90	19.8	541	72.0	0.94	1.70
320	112.9	0.1499								
340	146.1	0.1639								
360	186.7	0.1894								
370	210.5	0.2225								
374.15	221.2	0.317								

The values for saturated water can be used with good accuracy above saturation pressure. The values for saturated steam can be used with only moderate accuracy below saturation pressure at temperatures greater than 200 °C.

General Information for H₂O

Triple point: Thermodynamic temperature (by definition) =

$$273.16 \text{ K} \cong 0.01^\circ\text{C} \cong 491.688 \text{ R} \cong 32.018^\circ\text{F}$$

(hence $0^\circ\text{C} \cong 273.15 \text{ K}$, $0^\circ\text{F} \cong 459.67 \text{ R}$, $32^\circ\text{F} \cong 491.67 \text{ R}$)

Gas constant: $R = R_0/M = 8.3144/18.015 = 0.4615 \text{ kJ/kg K}$

Compressed Water

$t/^\circ\text{C}$		0.01	100	200	250	300	350	374.15
$p/[\text{bar}]$ ($t_s/^\circ\text{C}$)	p_s	0.006112	1.01325	15.55	39.78	85.92	165.4	221.2
	$v_f \times 10^3$	0.1000	0.1044	0.1157	0.1251	0.1404	0.1741	0.317
	h_f	0	419	852	1086	1345	1671	2084
	s_f	0	1.307	2.331	2.793	3.255	3.779	4.430
100 (311.0)	$(v-v_f) \times 10^3$	-0.0005	-0.0006	-0.0009	-0.0011	-0.0007		
	$(h-h_f)$	+10	+7	+4	0	-2		
	$(s-s_f)$	0.000	-0.008	-0.013	-0.014	-0.007		
221.2 (374.15)	$(v-v_f) \times 10^3$	-0.0011	-0.0012	-0.0020	-0.0029	-0.0051	-0.0107	0
	$(h-h_f)$	+22	+17	+9	+1	-12	-34	0
	$(s-s_f)$	+0.001	-0.017	-0.031	-0.040	-0.053	-0.071	0
500	$(v-v_f) \times 10^3$	-0.0023	-0.0024	-0.0042	-0.0064	-0.0117	-0.0298	-0.161
	$(h-h_f)$	+49	+38	+23	+8	-21	-94	-369
	$(s-s_f)$	0.000	-0.037	-0.068	-0.091	-0.134	-0.235	-0.670
1000	$(v-v_f) \times 10^3$	-0.0044	-0.0044	-0.0075	-0.0111	-0.0191	-0.0427	-0.180
	$(h-h_f)$	+96	+76	+51	+28	-17	-119	-415
	$(s-s_f)$	-0.007	-0.070	-0.124	-0.164	-0.235	-0.385	-0.853

Saturated Ice and Steam

t [$^\circ\text{C}$]	p_s [bar]	v_i [$10^{-3} \text{ m}^3/\text{kg}$]	v_g [m^3/kg]	u_i [kJ/kg]	u_g [kJ/kg]	h_i [kJ/kg]	h_g [kJ/kg]	s_i [kJ/kg K]	s_g [kJ/kg K]
0.01	0.006112	0.1091	206.1	-333.5	2374.7	-333.5	2500.8	-1.221	9.155
-10	0.002598	0.1089	467.5	-354.2	2360.8	-354.2	2482.2	-1.298	9.481
-20	0.001038	0.1087	1125	-374.1	2346.8	-374.1	2463.6	-1.375	9.835
-30	0.0003809	0.1086	2946	-393.3	2332.9	-393.3	2445.1	-1.452	10.221
-40	0.0001288	0.1084	8354	-411.8	2319.0	-411.8	2426.6	-1.530	10.644

Isentropic Expansion of Steam—Approximate Relations

Wet equilibrium expansion:

$pv^n = \text{constant}$, with $n \approx 1.125$ for steam initially dry saturated

Superheated and supersaturated expansion:

$pv^n = \text{constant}$ and $p/T^{n/(n-1)} = \text{constant}$, with $n \approx 1.3$

$$\text{Enthalpy drop} \frac{(h_2 - h_1)}{[\text{kJ/kg}]} = \left(\frac{h_1}{[\text{kJ/kg}]} - 1943 \right) \left[\left(\frac{p_2}{p_1} \right)^{(n-1)/n} - 1 \right]$$

Specific volume of supersaturated steam:

$$\frac{p}{[\text{bar}]} \times \frac{v}{[\text{m}^3/\text{kg}]} \times 10^2 = \frac{0.3}{1.3} \left(\frac{h}{[\text{kJ/kg}]} - 1943 \right)$$

Ammonia—NH₃ (Refrigerant 717)

Saturation Values						Superheat ($t - t_s$)			
						50 K		100 K	
t [°C]	p_s [bar]	v_g [m ³ /kg]	h_f h_g [kJ/kg]	s_f s_g [kJ/kg K]		h [kJ/kg]	s [kJ/kg K]	h [kJ/kg]	s [kJ/kg K]
-50	0.4089	2.625	-44.4 1373.3	-0.194 6.59		1479.8	6.592	1585.9	6.948
-45	0.5454	2.005	-22.3 1381.6	-0.096 6.57		1489.3	6.486	1596.1	6.839
-40	0.7177	1.552	0 1390.0	0 6.562		1498.6	6.387	1606.3	6.736
-35	0.9322	1.216	22.3 1397.9	0.095 6.572		1507.9	6.293	1616.3	6.639
-30	1.196	0.9633	44.7 1405.6	0.188 6.585		1517.0	6.203	1626.3	6.547
-28	1.317	0.8809	53.6 1408.5	0.224 6.581		1520.7	6.169	1630.3	6.512
-26	1.447	0.8058	62.6 1411.4	0.261 6.578		1524.3	6.135	1634.2	6.477
-24	1.588	0.7389	71.7 1414.3	0.297 6.586		1527.9	6.103	1638.2	6.444
-22	1.740	0.6783	80.8 1417.3	0.333 6.555		1531.4	6.071	1642.2	6.411
-20	1.902	0.6237	89.8 1420.0	0.368 6.523		1534.8	6.039	1646.0	6.379
-18	2.077	0.5743	98.8 1422.7	0.404 6.593		1538.2	6.008	1650.0	6.347
-16	2.265	0.5296	107.9 1425.3	0.440 6.563		1541.7	5.978	1653.8	6.316
-14	2.465	0.4890	117.0 1427.9	0.475 6.533		1545.1	5.948	1657.7	6.286
-12	2.680	0.4521	126.2 1430.5	0.510 6.504		1548.5	5.919	1661.5	6.256
-10	2.908	0.4185	135.4 1433.0	0.544 6.475		1551.7	5.891	1665.3	6.227
-8	3.153	0.3879	144.5 1435.3	0.579 6.447		1554.9	5.863	1669.0	6.199
-6	3.413	0.3599	153.6 1437.6	0.613 6.419		1558.2	5.836	1672.8	6.171
-4	3.691	0.3344	162.8 1439.9	0.647 6.392		1561.4	5.808	1676.4	6.143
-2	3.983	0.3110	172.0 1442.2	0.681 6.365		1564.6	5.782	1680.1	6.116
0	4.295	0.2895	181.2 1444.4	0.715 6.340		1567.8	5.756	1683.9	6.090
2	4.625	0.2699	190.4 1446.5	0.749 6.314		1570.9	5.731	1687.5	6.065
4	4.975	0.2517	199.7 1448.5	0.782 6.288		1574.0	5.706	1691.2	6.040
6	5.346	0.2351	209.1 1450.6	0.816 6.263		1577.0	5.682	1694.9	6.015
8	5.736	0.2198	218.5 1452.5	0.849 6.238		1580.1	5.658	1698.4	5.991
10	6.149	0.2056	227.8 1454.3	0.881 6.213		1583.1	5.634	1702.2	5.967
12	6.585	0.1926	237.2 1456.1	0.914 6.189		1586.0	5.611	1705.7	5.943
14	7.045	0.1805	246.6 1457.8	0.947 6.155		1588.9	5.588	1709.1	5.920
16	7.529	0.1693	256.0 1459.5	0.979 6.141		1591.7	5.565	1712.5	5.898
18	8.035	0.1590	265.5 1461.1	1.012 6.118		1594.4	5.543	1715.9	5.876
20	8.570	0.1494	275.1 1462.6	1.044 6.095		1597.2	5.521	1719.3	5.854
22	9.134	0.1405	284.6 1463.9	1.076 6.072		1600.0	5.499	1722.8	5.832
24	9.722	0.1322	294.1 1465.2	1.108 6.049		1602.7	5.478	1726.3	5.811
26	10.34	0.1245	303.7 1466.5	1.140 6.027		1605.3	5.458	1729.6	5.790
28	10.99	0.1173	313.4 1467.8	1.172 6.005		1608.0	5.437	1732.7	5.770
30	11.67	0.1106	323.1 1468.9	1.204 5.984		1610.5	5.417	1735.9	5.750
32	12.37	0.1044	332.8 1469.9	1.235 5.962		1613.0	5.397	1739.3	5.731
34	13.11	0.0986	342.5 1470.8	1.267 5.940		1615.4	5.378	1742.6	5.711
36	13.89	0.0931	352.3 1471.8	1.298 5.919		1617.8	5.358	1745.7	5.692
38	14.70	0.0880	362.1 1472.6	1.329 5.898		1620.1	5.340	1748.7	5.674
40	15.54	0.0833	371.9 1473.3	1.360 5.877		1622.4	5.321	1751.9	5.655
42	16.42	0.0788	381.8 1473.8	1.391 5.856		1624.6	5.302	1755.0	5.637
44	17.34	0.0746	391.8 1474.2	1.422 5.835		1626.8	5.284	1758.0	5.619
46	18.30	0.0706	401.8 1474.5	1.453 5.814		1629.0	5.266	1761.0	5.602
48	19.29	0.0670	411.9 1474.7	1.484 5.793		1631.1	5.248	1764.0	5.584
50	20.33	0.0635	421.9 1474.7	1.515 5.773		1633.1	5.230	1766.8	5.567

Critical point $t_c = 132.4$ °C, $p_c = 113.0$ bar.Molar mass $M = 17.030$ kg/kmol; further properties of the liquid are given on p. 15.

Dichlorodifluoromethane - CF_2Cl_2 (Refrigerant 12)

Saturation Values						Superheat ($t-t_s$)				
t [°C]	p_s [bar]	v_g [m³/kg]	h_f h_g		s_f s_g		15 K		30 K	
			[kJ/kg]		[kJ/kg K]		h	s	h	s
							[kJ/kg]	[kJ/kg K]	[kJ/kg]	[kJ/kg K]
-100	0.0118	10.100	-51.84	142.00	-0.2567	0.8628	148.89	0.9019	156.10	0.9428
-95	0.0181	6.585	-47.56	144.22	-0.2323	0.8442	151.23	0.8830	158.55	0.9195
-90	0.0284	4.416	-43.28	146.46	-0.2086	0.8274	153.59	0.8649	161.02	0.9010
-85	0.0424	3.037	-39.00	148.73	-0.1856	0.8122	155.98	0.8493	163.52	0.8851
-80	0.0617	2.138	-34.72	151.02	-0.1631	0.7985	158.39	0.8351	166.04	0.8706
-75	0.0879	1.538	-30.43	153.32	-0.1412	0.7861	160.82	0.8226	168.57	0.8578
-70	0.1227	1.127	-26.13	155.62	-0.1198	0.7749	163.26	0.8110	171.12	0.8459
-65	0.1680	0.8412	-21.81	157.91	-0.0988	0.7649	165.70	0.8008	173.68	0.8355
-60	0.2262	0.6379	-17.49	160.21	-0.0783	0.7558	168.15	0.7915	176.26	0.8259
-55	0.2998	0.4910	-13.14	162.61	-0.0582	0.7475	170.60	0.7830	178.84	0.8172
-50	0.3915	0.3831	-8.78	164.91	-0.0384	0.7401	173.07	0.7753	181.43	0.8093
-45	0.5044	0.3027	-4.40	167.24	-0.0190	0.7335	175.54	0.7685	184.01	0.8023
-40	0.6417	0.2419	0	169.60	0	0.7274	178.00	0.7623	186.60	0.7959
-35	0.8071	0.1954	4.42	171.90	0.0187	0.7219	180.45	0.7568	189.18	0.7902
-30	1.004	0.1594	8.86	174.20	0.0371	0.7170	182.90	0.7517	191.76	0.7851
-25	1.217	0.1312	13.33	176.48	0.0552	0.7127	185.33	0.7473	194.33	0.7805
-20	1.509	0.1088	17.82	178.71	0.0711	0.7087	187.75	0.7432	196.89	0.7764
-15	1.826	0.0910	22.33	180.97	0.0906	0.7051	190.15	0.7397	199.44	0.7728
-10	2.191	0.0766	26.87	183.19	0.1080	0.7020	192.53	0.7365	201.97	0.7695
-5	2.610	0.0650	31.45	185.38	0.1251	0.6991	194.90	0.7336	204.49	0.7666
0	3.086	0.0554	36.05	187.53	0.1420	0.6966	197.25	0.7311	206.99	0.7641
5	3.626	0.0475	40.69	189.66	0.1587	0.6943	199.56	0.7289	209.47	0.7618
10	4.233	0.0409	45.37	191.74	0.1752	0.6921	201.85	0.7268	211.92	0.7598
15	4.914	0.0354	50.10	193.78	0.1915	0.6901	204.10	0.7251	214.35	0.7580
20	5.673	0.0308	54.87	195.78	0.2078	0.6885	206.32	0.7235	216.75	0.7565
25	6.516	0.0269	59.70	197.73	0.2239	0.6869	208.50	0.7220	219.11	0.7552
30	7.449	0.0235	64.59	199.62	0.2399	0.6853	210.63	0.7208	221.44	0.7540
35	8.477	0.0206	69.55	201.45	0.2559	0.6839	212.72	0.7196	223.73	0.7529
40	9.607	0.0182	74.59	203.20	0.2718	0.6825	214.76	0.7185	225.98	0.7519
45	10.84	0.0160	79.71	204.87	0.2877	0.6811	216.74	0.7175	228.18	0.7511
50	12.19	0.0142	84.94	206.45	0.3037	0.6797	218.64	0.7166	230.33	0.7503
55	13.66	0.0125	90.27	207.92	0.3197	0.6782	220.48	0.7156	232.42	0.7496
60	15.26	0.0111	95.74	209.26	0.3358	0.6765	222.23	0.7146	234.45	0.7490
65	16.99	0.00985	101.36	210.46	0.3521	0.6747	223.89	0.7136	236.42	0.7484
70	18.86	0.00873	107.15	211.48	0.3686	0.6726	225.45	0.7125	238.32	0.7477
75	20.88	0.00772	113.15	212.29	0.3854	0.6702	226.89	0.7113	240.13	0.7470
80	23.05	0.00682	119.39	212.83	0.4027	0.6673	228.21	0.7099	241.86	0.7463
85	25.38	0.00601	125.93	213.04	0.4204	0.6636	229.39	0.7084	243.50	0.7455
90	27.89	0.00526	132.84	212.80	0.4389	0.6591	230.43	0.7067	245.03	0.7445
95	30.57	0.00456	140.23	211.94	0.4583	0.6531	231.30	0.7047	246.47	0.7435
100	33.44	0.00390	148.32	210.12	0.4793	0.6449	231.93	0.7023	247.80	0.7424
105	36.51	0.00324	157.52	206.57	0.5028	0.6325	232.22	0.6994	248.97	0.7412
110	39.79	0.00246	169.55	197.99	0.5334	0.6076	232.47	0.6964	250.10	0.7399
112	41.15	0.00179	183.43	83.43	0.5690	0.5690	232.80	0.6958	250.58	0.7394

Molar mass $M = 120.91 \text{ kg/kmol}$; further properties of the liquid are given on p. 15.

Mercury - Hg

p [bar]	t_s [°C]	v_f [m³/kg]	h_f	h_{fg} [kJ/kg]	h_g	s_f	s_{fg} [kJ/kg K]	s_g
0.0006	109.2	259.6	15.13	297.20	312.33	0.0466	0.7774	0.8240
0.0007	112.3	224.3	15.55	297.14	312.69	0.0477	0.7709	0.8186
0.0008	115.0	197.7	15.93	297.09	313.02	0.0487	0.7654	0.8141
0.0009	117.5	176.8	16.27	297.04	313.31	0.0496	0.7604	0.8100
0.0010	119.7	160.1	16.58	297.00	313.58	0.0503	0.7560	0.8063
0.002	134.9	83.18	18.67	296.71	315.38	0.0556	0.7271	0.7827
0.004	151.5	43.29	20.93	296.40	317.33	0.0610	0.6981	0.7591
0.006	161.8	29.57	22.33	296.21	318.54	0.0643	0.6811	0.7454
0.008	169.4	22.57	23.37	296.06	319.43	0.0666	0.6690	0.7356
0.010	175.5	18.31	24.21	295.95	320.16	0.0685	0.6596	0.7281
0.02	195.6	9.570	26.94	295.57	322.51	0.0744	0.6305	0.7049
0.04	217.7	5.013	29.92	295.15	325.07	0.0806	0.6013	0.6819
0.06	231.6	3.438	31.81	294.89	326.70	0.0843	0.5842	0.6685
0.08	242.0	2.632	33.21	294.70	327.91	0.0870	0.5721	0.6591
0.10	250.3	2.140	34.33	294.54	328.87	0.0892	0.5627	0.6519
0.2	278.1	1.128	38.05	294.02	332.07	0.0961	0.5334	0.6295
0.4	309.1	0.5942	42.21	293.43	335.64	0.1034	0.5039	0.6073
0.6	329.0	0.4113	44.85	293.06	337.91	0.1078	0.4869	0.5947
0.8	343.9	0.3163	46.84	292.78	339.62	0.1110	0.4745	0.5855
1	356.1	0.2581	48.45	292.55	341.00	0.1136	0.4649	0.5785
2	397.1	0.1377	53.87	291.77	345.64	0.1218	0.4353	0.5571
3	423.8	0.09551	57.38	291.27	348.65	0.1268	0.4179	0.5447
4	444.1	0.07378	60.03	290.89	350.92	0.1305	0.4056	0.5361
5	460.7	0.06044	62.20	290.58	352.78	0.1334	0.3960	0.5294
6	474.9	0.05137	64.06	290.31	354.37	0.1359	0.3881	0.5240
7	487.3	0.04479	65.66	290.08	355.74	0.1380	0.3815	0.5195
8	498.4	0.03978	67.11	289.87	356.98	0.1398	0.3757	0.5155
9	508.5	0.03584	68.42	289.68	358.10	0.1415	0.3706	0.5121
10	517.8	0.03266	69.61	289.50	359.11	0.1429	0.3660	0.5089
12	534.4	0.02781	71.75	289.19	360.94	0.1455	0.3581	0.5036
14	549.0	0.02429	73.63	288.92	362.55	0.1478	0.3514	0.4992
16	562.0	0.02161	75.37	288.67	364.04	0.1498	0.3456	0.4954
18	574.0	0.01949	76.83	288.45	365.28	0.1515	0.3405	0.4920
20	584.9	0.01778	78.23	288.24	366.47	0.1531	0.3359	0.4890
22	595.1	0.01637	79.54	288.05	367.59	0.1546	0.3318	0.4864
24	604.6	0.01518	80.75	287.87	368.62	0.1559	0.3280	0.4839
26	613.5	0.01416	81.89	287.70	369.59	0.1571	0.3245	0.4816
28	622.0	0.01329	82.96	287.54	370.50	0.1583	0.3212	0.4795
30	630.0	0.01252	83.97	287.39	371.36	0.1594	0.3182	0.4776
35	648.5	0.01096	86.33	287.04	373.37	0.1619	0.3115	0.4734
40	665.1	0.00978	88.43	286.73	375.16	0.1641	0.3056	0.4697
45	680.3	0.00885	90.35	286.44	376.79	0.1660	0.3004	0.4664
50	694.4	0.00809	92.11	286.18	378.29	0.1678	0.2958	0.4636
55	707.4	0.00746	93.76	285.93	379.69	0.1694	0.2916	0.4610
60	719.7	0.00693	95.30	285.70	381.00	0.1709	0.2878	0.4587
65	731.3	0.00648	96.75	285.48	382.23	0.1723	0.2842	0.4565
70	742.3	0.00609	98.12	285.23	383.40	0.1736	0.2809	0.4545
75	752.7	0.00575	99.42	285.03	384.50	0.1748	0.2779	0.4527

h_f and s_f are zero at 0 °C. Molar mass $M = 200.59$ kg/kmol; for superheated vapour $c_p = 0.1036$ kJ/kg K; further properties of the liquid are given on p. 15.